

Homework 4 solutions

①

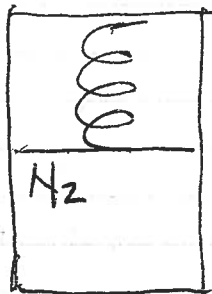
1. Relation $\Delta U = mC_v(\Delta T)$ applies to any process with ideal gas

2. Relation $\Delta H = mC_p(\Delta T)$ applies to any process with ideal gas

3. Both require the same energy: $\Delta U = mC_v(T_2 - T_1)$
(volume not a factor)

4. Both require the same energy: $\Delta H = mC_p(T_2 - T_1)$
(pressure not a factor)

5.



$$m = 10 \text{ g} \times 10^{-3} \frac{\text{kg}}{\text{g}} = 0.01 \text{ kg}$$

$$P_1 = 120 \text{ kPa}$$

$$T_1 = 27^\circ\text{C} + 273 = 300 \text{ K}$$

$$R = 0.2968 \text{ kJ/kgK}$$

$$\text{Spring constant } k = 1 \frac{\text{KN}}{\text{m}}$$

$$d_p = 10 \text{ cm} \times 10^{-2} \frac{\text{m}}{\text{cm}}$$

$$d_p = 0.1 \text{ m}$$

$$A_p = \frac{\pi (0.1 \text{ m})^2}{4}$$

$$A_p = 0.00785 \text{ m}^2$$

Hook's Law $F_s = kx$ where x = displacement (m)

$$\text{solution } \Delta U = mC_v(T_2 - T_1)$$

$$\Delta H = mC_p(T_2 - T_1)$$

$$\text{need } T_2 \text{ from } P_2 V_2 = mRT_2 \Rightarrow T_2 = \frac{P_2 (1.4 V_1)}{mR}$$

need P_2 to solve
and V_1

$$5. P_1 = P_2 + \frac{F_s}{A} = P_1 + \frac{kx}{A} \quad (2)$$

$$x = \frac{V_2 - V_1}{A} = 0.1 \frac{V_1}{A} = \frac{0.1 V_1}{0.00785 \text{ m}^2}$$

$$V_1 = \frac{mRT_1}{P_1} = \frac{0.01 \text{ kg} (0.2968 \text{ kJ/kgK}) (300 \text{ K})}{120 \text{ kPa}} = 0.00742 \text{ m}^3$$

$$x = \frac{0.1 (0.00742) \text{ m}^3}{0.00785 \text{ m}^2} = 0.0945 \text{ m}$$

$$P_2 = 120 \text{ kPa} + \frac{1 \text{ kN}}{\text{m}} \frac{(0.0945 \text{ m})}{0.00785 \text{ m}^2} = 120 + 12 \text{ kPa}$$

$$T_2 = \frac{132 \text{ kPa} (1.1) (0.00742 \text{ m}^3)}{0.01 \text{ kg} (0.2968 \text{ kJ/kgK})} = 363.1 \text{ K}$$

$$C_v @ 300 \text{ K} = 0.743 \text{ kJ/kgK} \quad C_p = 1.04 \text{ kJ/kgK}$$

$$\Delta U = m C_v (T_2 - T_1) = 0.01 \text{ kg} (0.743 \frac{\text{kJ}}{\text{kgK}}) (363.1 - 300) \text{ K}$$

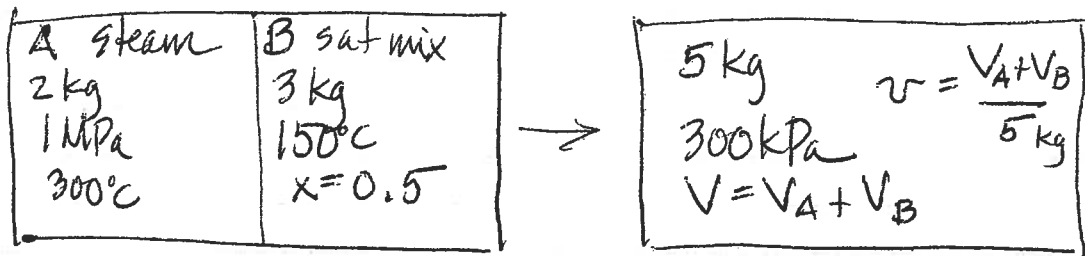
$$\boxed{\Delta U = 0.47 \text{ kJ}}$$

$$\Delta H = m C_p (T_2 - T_1)$$

$$\Delta H = 0.01 \text{ kg} (1.04 \frac{\text{kJ}}{\text{kgK}}) (363.1 - 300 \text{ K})$$

$$\boxed{\Delta H = 0.66 \text{ kJ}}$$

6.



3

A. steam is superheated ($T > T_s @ 1 \text{ MPa}$)

$$v_A = 0.25799 \text{ m}^3/\text{kg} \quad (\text{A-6})$$

$$V_A = 2 \text{ kg} \left(0.25799 \frac{\text{m}^3}{\text{kg}} \right) = 0.516 \text{ m}^3$$

B. $v_B = 0.5(v_g - v_f) + v_f @ 150^\circ\text{C} \quad (\text{A-4})$

$$= 0.5(0.39248 - 0.001091) + 0.001091 = 0.1968 \frac{\text{m}^3}{\text{kg}}$$

$$V_B = 3 \text{ kg} \left(0.1968 \frac{\text{m}^3}{\text{kg}} \right) = 0.59 \text{ m}^3$$

state 2

$$v = \frac{V_A + V_B}{5 \text{ kg}} = \frac{0.516 + 0.59}{5} \text{ m}^3$$

$$v_2 = 0.2213 \frac{\text{m}^3}{\text{kg}} @ 300 \text{ kPa}$$

$$v_f < v_2 < v_g \Rightarrow \text{sat. mixture}$$

a) $T = T_{\text{sat}} = \boxed{133.52^\circ\text{C}}$

b) $h_A = 3051.6 \text{ kJ/kg} \quad (\text{A-6})$

$$H_A = 2 \text{ kg} (3051.6 \frac{\text{kJ}}{\text{kg}}) = 6103.2 \text{ kJ}$$

$$h_B = 0.5(2113.8) + 0.5(3218) = 1689.1 \frac{\text{kJ}}{\text{kg}}$$

$$H_B = 3 \text{ kg} (1689.1 \frac{\text{kJ}}{\text{kg}}) = 5067.2 \text{ kJ}$$

6. $H_A + H_B = 6103.2 + 5067.2 \text{ kJ} = 11,170.4 \text{ kJ}$

$h_2 = x(h_{fg}) + h_f @ 300 \text{ kPa}$

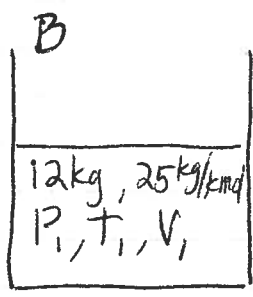
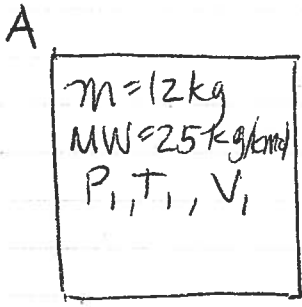
$x = \frac{v_2 - v_f}{v_{fg}} = \frac{0.2213 - 0.001093}{0.60582 - 0.001073} = 0.364$

$h_2 = 0.364(2163.5) + 561.43 = 1349.3 \text{ kJ/kg}$

$H_2 = 5 \text{ kg} (1349.3) \text{ kJ/kg} = 6,746.5 \text{ kJ}$

$\Delta H = 6746.5 - 11170.4 = -4424 \text{ kJ (LOST)}$

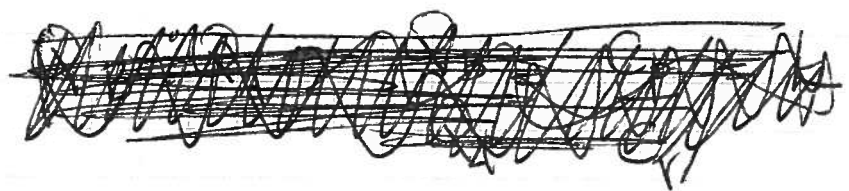
7.



$\Delta T = 15^\circ \text{C}$

$Q_A = mC_v(\Delta T)$

$Q_B = mC_p \Delta T$



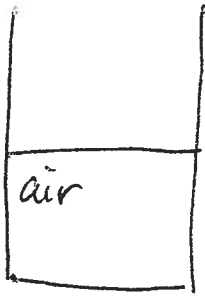
extra heat = $Q_B - Q_A = mC_p \Delta T - mC_v \Delta T$

$Q_B - Q_A = m \Delta T (C_p - C_v)$

$C_p - C_v = R \quad R = \frac{R_u}{25} = \frac{8.314}{25} = 0.333 \text{ kJ/kgK}$

$Q_A - Q_B = 12 \text{ kg} (15 \text{ K}) 0.333 \text{ kJ/kgK} = 60 \text{ kJ more}$

8.



air compressed
 $m = 2.4 \text{ kg}$

$$P_1 = 150 \text{ kPa}$$

$$P_2 = 600 \text{ kPa}$$

$$T_1 = 12^\circ\text{C} = 285 \text{ K} = T_2$$

4a

isothermal work, ideal gas

$$P_1 V_1 = P_2 V_2$$

$$W_b = mRT \ln\left(\frac{P_1}{P_2}\right)$$

$$\frac{V_2}{V_1} = \frac{P_1}{P_2}$$

$$W_b = 2.4 \text{ kg} \left(0.287 \frac{\text{kJ}}{\text{kg}\cdot\text{K}} \right) \left(\ln\left(\frac{150}{600}\right) \right) (285 \text{ K})$$

$$W_b = -272.1 \text{ kJ}$$

9. N_2 expanded as $PV^n = C$

$$V_1 = 2 \text{ m}^3$$

$$V_2 = 6 \text{ m}^3$$

$$P_1 = 500 \text{ kPa}$$

$$P_2 = 250 \text{ kPa}$$

$$T_1 = 300^\circ\text{C} = 573 \text{ K}$$

a) find n

$$P_1 V_1^n = P_2 V_2^n$$

$$\frac{P_1}{P_2} = \left(\frac{V_2}{V_1}\right)^n$$

$$\ln\left(\frac{P_1}{P_2}\right) = n \ln\left(\frac{V_2}{V_1}\right) = n \ln(3)$$

$$\ln(2) = n \ln(3)$$

$$n = \frac{\ln(2)}{\ln(3)} = \boxed{0.631}$$

b) find T_2

ideal gas

$$\frac{P_1 V_1}{T_1} = \frac{P_2 V_2}{T_2}$$

$$T_2 = \left(\frac{P_2}{P_1}\right) \left(\frac{V_2}{V_1}\right) T_1$$

$$T_2 = (0.5)(3)(573 \text{ K}) = \boxed{860 \text{ K}}$$

OR $\boxed{T_2 = 587^\circ\text{C}}$

(5)

$$9 c) \text{ find } W_b = \frac{P_2 V_2 - P_1 V_1}{(1-\eta)} = \frac{250(6) - 500(2)}{1-0.631} \quad (6)$$

$$W_b = 1,355 \text{ kJ}$$

$$10. a) 1 \rightarrow 2 \quad P_1 V_1 = P_2 V_2$$

$$P_2 = P_1 \frac{V_1}{V_2} = 100 \text{ kPa} (3) \quad \boxed{= 300 \text{ kPa}}$$

$$b) P_3 = 100/2 = 50 \text{ kPa} = P_4$$

$$W_{b34} = P (V_4 - V_3) = 50 \text{ kPa} (3 - 1) \text{ m}^3$$

$$W_{b34} = \boxed{100 \text{ kJ}}$$

$$c) W_{b12} = P_1 V_1 \ln\left(\frac{V_2}{V_1}\right) = 300 \text{ kPa} (1 \text{ m}^3) \ln\left(\frac{1}{3}\right)$$

$$W_{b12} = -330 \text{ kJ}$$

$$d) W_{\text{net}} = W_{b34} + W_{b12} \quad (\text{no } W_b \text{ for } 2 \rightarrow 3 \text{ or } 4 \rightarrow 1)$$

$$= 100 \text{ kJ} - 330 \text{ kJ} = \boxed{-230 \text{ kJ}}$$

Graph next page

9. Nitrogen, an ideal gas, is expanded in a polytropic process according to the relation:

$$PV^n = \text{constant}$$

where P = pressure (kPa), V = volume (m^3) and n = a constant. The initial volume of the nitrogen is $2 m^3$; the initial pressure is 500 kPa and the initial temperature is $300^\circ C$. During the expansion, the volume triples and the pressure decreases to half its initial value.

- a. (1 point) Find n .
- b. (1 point) Calculate the equilibrium temperature after expansion.
- c. (1 point) Calculate the boundary work by the gas during the process in kJ.

10. A device containing air is operated in a cycle consisting of four processes with no work exchanges other than boundary work.

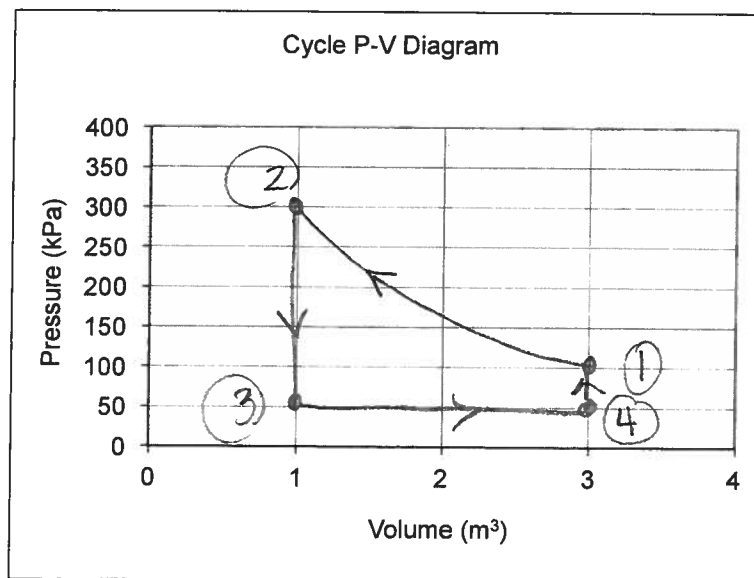
1 \rightarrow 2: Isothermal compression, $V_1 = 3 m^3$, $V_2 = 1 m^3$; $P_1 = 100 kPa$

2 \rightarrow 3: Isochoric heat loss, $P_3 = \frac{P_2}{2}$

3 \rightarrow 4: Isobaric expansion, $V_4 = 3 m^3$

4 \rightarrow 1: Isochoric heat addition, return to state 1

- a. (1 point) Find P_2
- b. (1 point) Find W_b for process 3 \rightarrow 4
- c. (1 point) Find W_b for process 1 \rightarrow 2
- d. (1 point) Find the net work for the cycle
- e. (1 point) Graph the process on the P-V diagram below



11. free body diagram on piston : $F_{H_2O} = F_{He}$

(9)

$$P_{H_2O} A_2 = P_{He} A_1$$

condensing water is saturated mixture @ $T = 200^\circ\text{C}$

$$P = P_{sat} = 1,555 \text{ kPa}$$

$$P_{He} = P_{H_2O} \left(\frac{A_2}{A_1} \right) \text{ where } \frac{A_2}{A_1} = \frac{d_2^2}{d_1^2} = \frac{4^2}{10^2} = 0.16$$

$$P_{He} = 1555 \text{ kPa} (0.16) = 249 \text{ kPa}$$

$$V_{He} = \frac{mRT}{P_{He}} = \frac{1 \text{ kg} (2.0769 \text{ kJ/kgK}) (200+273) \text{ K}}{249 \text{ kPa}}$$

$$\boxed{V_{He} = 3.95 \text{ m}^3}$$